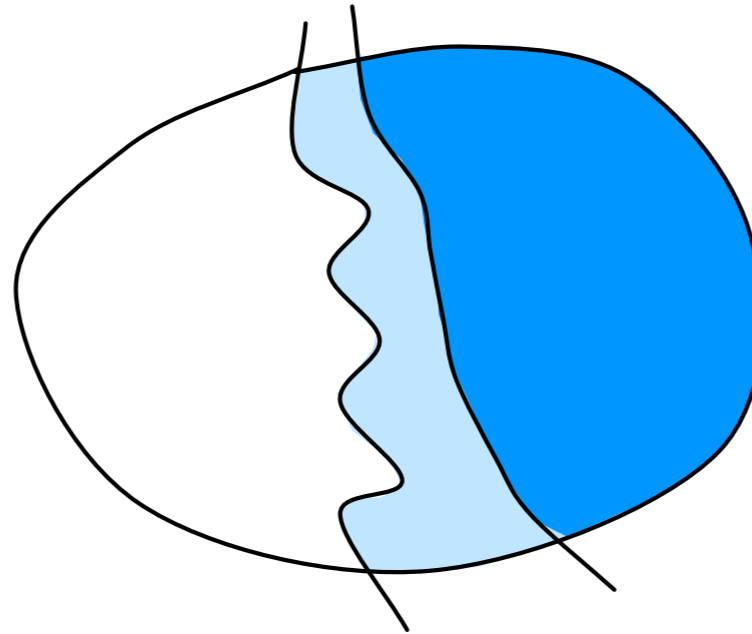


solid mush liquid



Enthalpy Method

Introduction

M.S Darwish

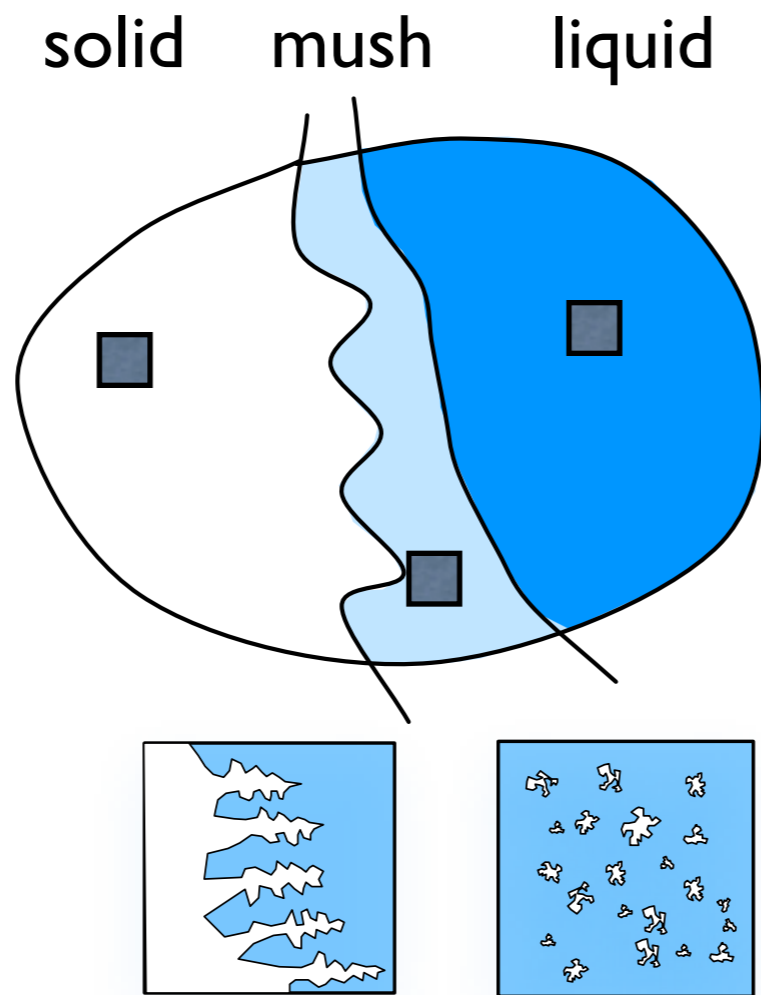
MECH 636: Solidification Modelling

The Mushy Zone

Conservation of Energy

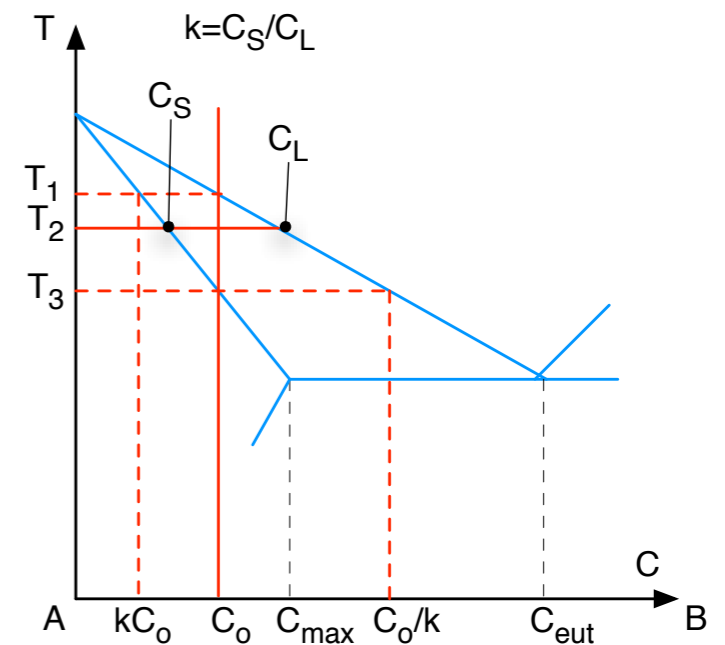
$$\frac{\partial(\rho^s h^s)}{\partial t} = \nabla \cdot (k^s \nabla T) + (\text{Interface term})^s$$

$$h^s = \int_{T_{ref}}^T c^s dT$$



$$\frac{\partial(\rho^l h^l)}{\partial t} + \nabla \cdot (\rho^l \mathbf{v}^l h^l) = \nabla \cdot (k^l \nabla T) + (\text{Interface term})^l$$

$$h^l = \int_{T_{ref}}^T c^l dT + L$$

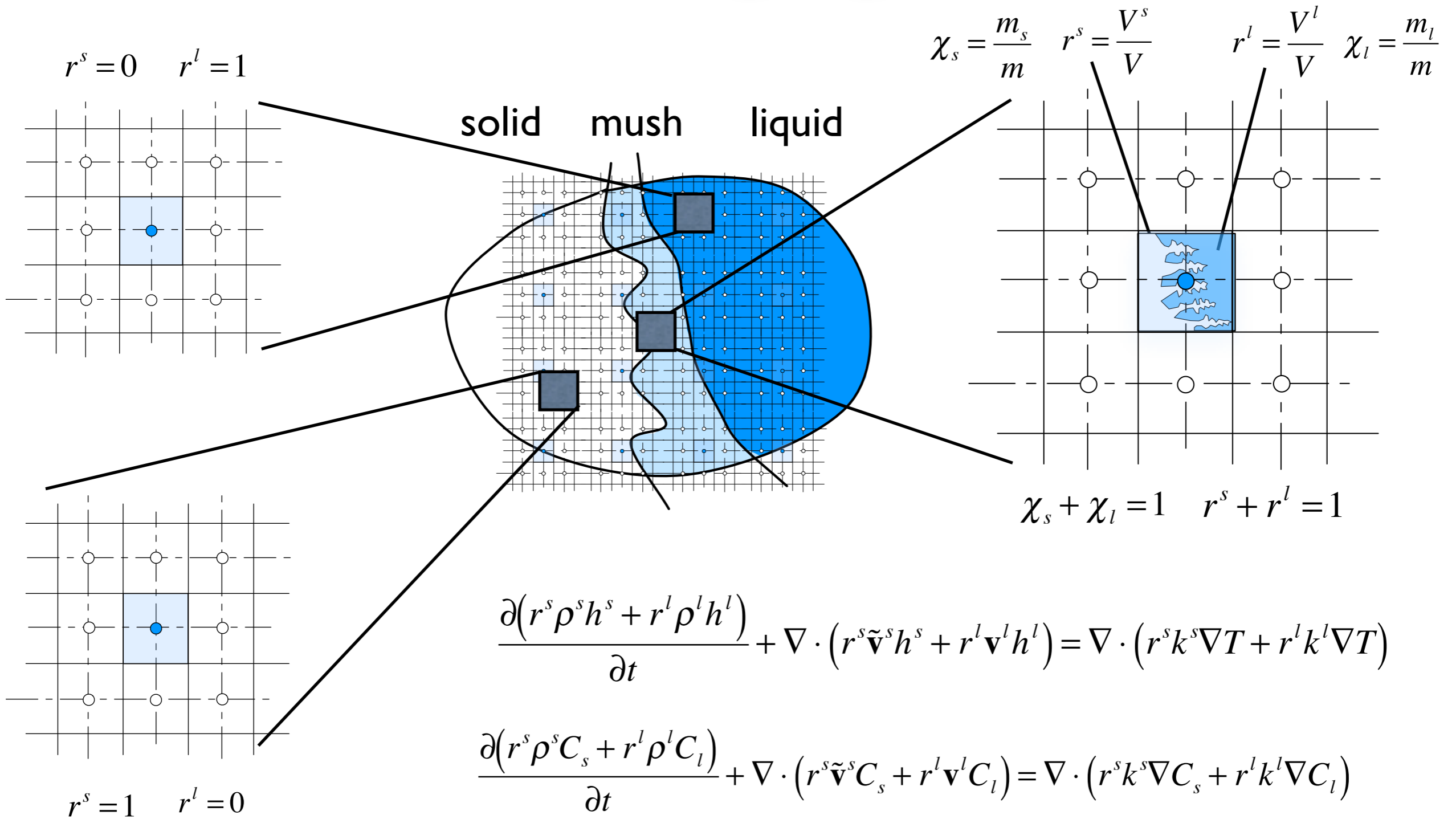


Conservation of Specie

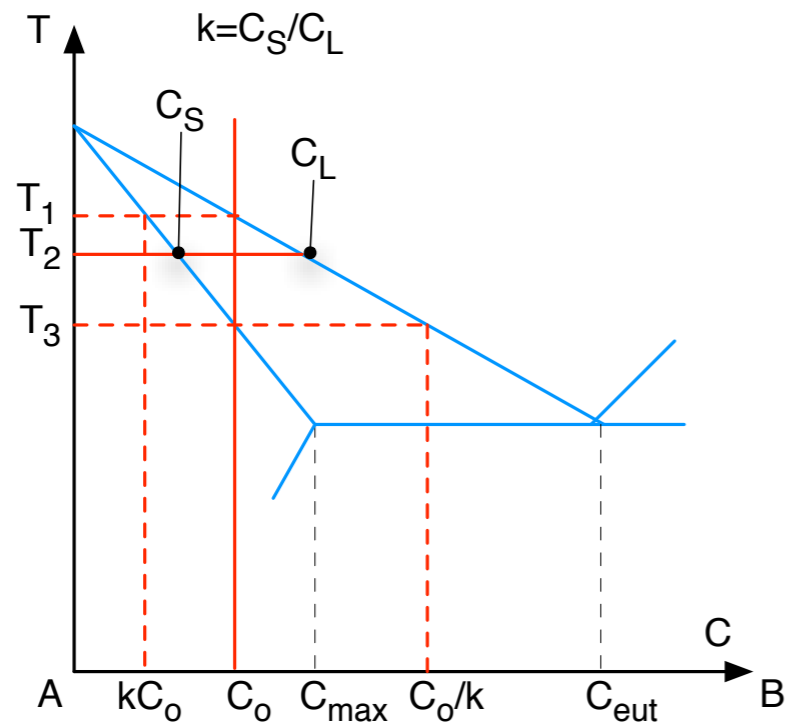
$$\frac{\partial(\rho^s C_s)}{\partial t} = \nabla \cdot (D^s \nabla C_s)$$

$$\frac{\partial(\rho^l C_l)}{\partial t} + \nabla \cdot (\rho^l \mathbf{v}^l C_l) = \nabla \cdot (D^l \nabla C_l)$$

Averaging



Mass and Volume Fractions



mass fraction

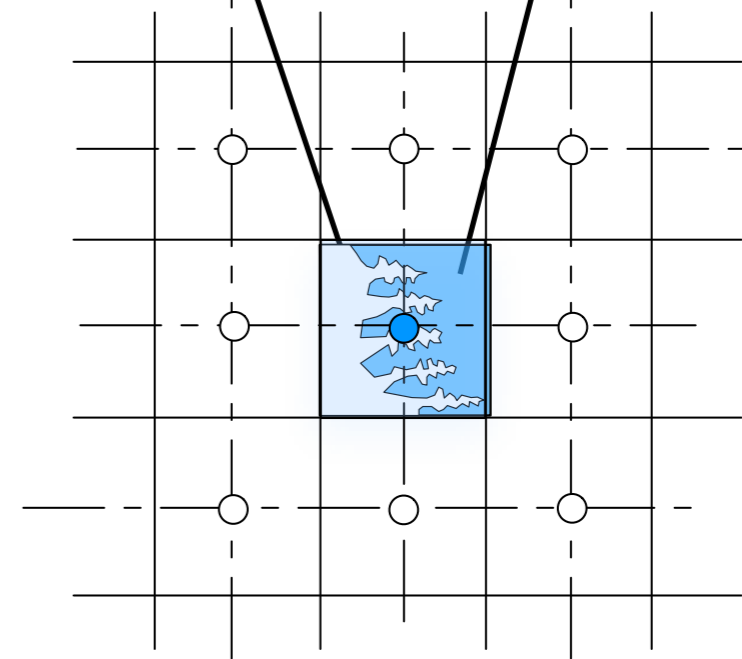
$$\chi_s = \frac{C_l - C_o}{C_l - C_s} = \frac{m_s}{m}$$

volume fraction

$$r_s = \frac{V_s}{V}$$

$$\frac{\chi_s}{r_s} = \frac{m_s}{m} \times \frac{V}{V_s} = \frac{\rho_s}{\rho}$$

$$\chi_s = \frac{m_s}{m} \quad r^s = \frac{V^s}{V} \quad r^l = \frac{V^l}{V} \quad \chi_l = \frac{m_l}{m}$$

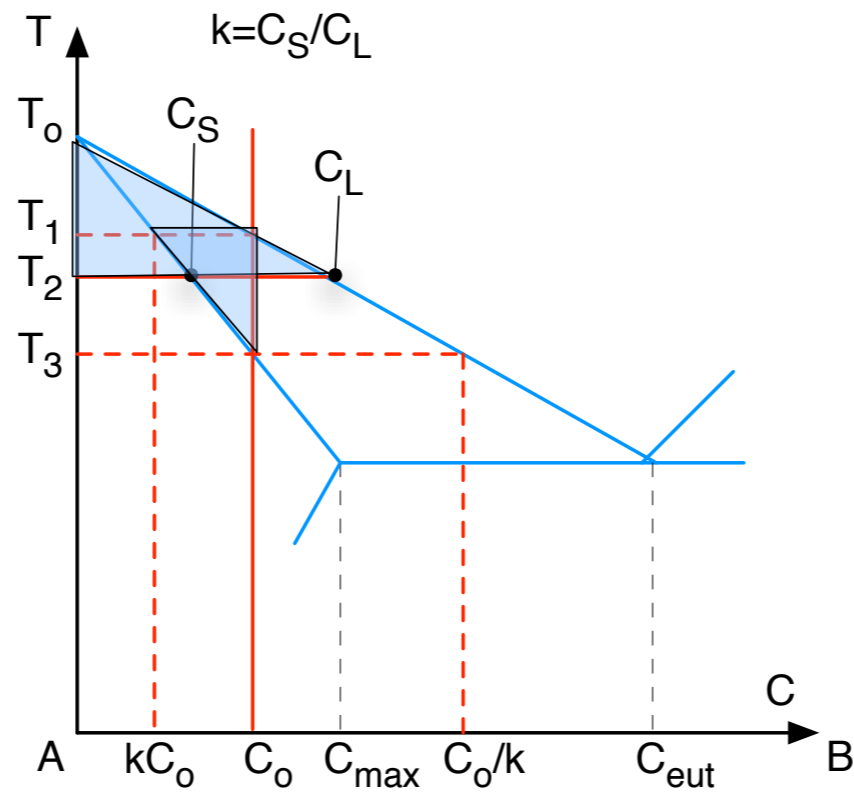


$$\chi_s + \chi_l = 1 \quad r^s + r^l = 1$$

$$r_s = \chi_s \frac{\rho}{\rho_s} = \frac{C_l - C_o}{C_l - C_s} \frac{\rho}{\rho_s}$$

$$r_l = \chi_l \frac{\rho}{\rho_l} = \frac{C_o - C_s}{C_l - C_s} \frac{\rho}{\rho_l}$$

Equilibrium Relations



$$\frac{C_l}{C_o} = \frac{T_1 - T_2}{T_0 - T_2}$$

$$\frac{C_o - C_s}{C_o - kC_o} = \frac{T_2 - T_3}{T_1 - T_3}$$

$$\chi_s = \frac{C_l - C_o}{C_l - C_s} = \frac{m_s}{m}$$

$$C_l = C_o \frac{T_0 - T_2}{T_0 - T_1}$$

$$C_s = C_o \left(1 - (1 - k) \frac{T_2 - T_3}{T_1 - T_3} \right)$$

$$\chi_s = \frac{T_1 - T_2}{(1 - k)(T_0 - T_2)}$$

$$r_s = \frac{T_1 - T_2}{(1 - k)(T_0 - T_2)} \left(\frac{\rho}{\rho_s} \right)$$

Average Energy Equations

$$T_{ref} = 0 \quad \frac{\partial(r_s \rho_s h_s + r_l \rho_l h_l)}{\partial t} + \nabla \cdot (r_s \rho_s \tilde{\mathbf{v}}_s h_s + r_l \rho_l \mathbf{v}_l h_l) = \nabla \cdot (r_s k_s \nabla T + r_l k_l \nabla T)$$

$$\textcircled{1} \quad r_s \rho_s h_s + r_l \rho_l h_l = r_s \rho_s \int_{T_{ref}}^T c_{p,s} dT + r_l \rho_l \left(\int_{T_{ref}}^T c_{p,l} dT + \delta H \right)$$

$$= \rho_m \int_{T_{ref}}^T c_{p,s} dT + r_l \rho_l \delta H$$

mixture

$$h_l = \int_{T_{ref}}^T c_{p,l} dT + L$$

$$= \int_{T_{ref}}^T c_{p,s} dT + \delta H$$

$$\delta H = \int_{T_{ref}}^T (c_{p,l} - c_{p,s}) dT + L$$

$$\textcircled{2} \quad r_s \rho_s \tilde{\mathbf{v}}_s h_s + r_l \rho_l \mathbf{v}_l h_l = r_s \rho_s \tilde{\mathbf{v}}_s \int_{T_{ref}}^T C_s dT + r_l \rho_l \mathbf{v}_l \left(\int_{T_{ref}}^T C_s dT + \delta H \right)$$

$$= r_m \rho_m \mathbf{v}_m \int_{T_{ref}}^T C_s dT + r_l \rho_l \mathbf{v}_l \delta H$$

mixture

$$\rho_m = r_s \rho_s + r_l \rho_l$$

$$\mathbf{v}_m = \frac{r_s \rho_s \tilde{\mathbf{v}}_s + r_l \rho_l \mathbf{v}_l}{r_m \rho_m}$$

$$\textcircled{3} \quad r_s k_s \nabla T + r_l k_l \nabla T = k_m \nabla T$$

mixture

$$k_m = r_s k_s + r_l k_l$$

Assumptions

$$\int_{T_{ref}}^T C dT \approx C \int_{T_{ref}}^T dT$$

$$T_{ref} = 0$$

$$\frac{\partial(\rho_m c_{p,s} T + r_l \rho_l \delta H)}{\partial t} + \nabla \cdot (\rho_m \mathbf{v}_m T + r_l \rho_l \mathbf{v}_l L) = \nabla \cdot (k_m \nabla T)$$

Neglecting Convection

$$\frac{\partial(\rho_m c_{p,s} T)}{\partial t} = \nabla \cdot (k_m \nabla T) - \frac{\partial(r_l \rho_l \delta H)}{\partial t}$$

Discretizing

$$\frac{\rho_m c_{p,s} T_P V_P - \overset{\text{old}}{\rho_m c_{p,s} T_P}}{\Delta t} = \sum_{f=nb(P)} (k_m \nabla T \cdot d\mathbf{S})_f - \frac{r_l \rho_l \delta H_P - \overset{\text{old}}{r_l \rho_l \delta H_P}}{\Delta t}$$

Algebraic Form

$$a_P T_P = \sum_{NB(P)} a_{NB} T_{NB} + b_P + a_P^t T_P^{\bullet} - \frac{V \rho_l \delta H}{\Delta t} (r_{l,P} - r_{l,P}^{\bullet})$$

Average Specie Equation

$$\frac{\partial(r_s \rho_s C_s + r_l \rho_l C_l)}{\partial t} + \nabla \cdot (r_s \rho_s \tilde{\mathbf{v}}_s C_s + r_l \rho_l \mathbf{v}_l C_l) = \nabla \cdot (r_s D_s \nabla C_s + r_l D_l \nabla C_l)$$

1

$$r_s \rho_s C_s + r_l \rho_l C_l = \rho_m C_m$$

mixture

$$C_m = \frac{r_s \rho_s C_s + r_l \rho_l C_l}{\rho_m}$$

2

$$r_s \rho_s \tilde{\mathbf{v}}_s C_s + r_l \rho_l \mathbf{v}_l C_l = (r_s \rho_s \tilde{\mathbf{v}}_s k + r_l \rho_l \mathbf{v}_l) C_l = \rho_m \mathbf{v}_m C_l$$

mixture

$$\mathbf{v}_m = \frac{r_s \rho_s \tilde{\mathbf{v}}_s k + r_l \rho_l \mathbf{v}_l}{\rho_m}$$

3

$$r_s D_s \nabla C_s + r_l D_l \nabla C_l = r_s D_s \nabla(k C_l) + r_l D_l \nabla C_l = D_m \nabla C_l$$

mixture

$$D_m = r_s k D_s + r_l D_l$$

$$\frac{\partial(\rho_m C_m)}{\partial t} + \nabla \cdot (\rho_m \mathbf{v}_m C_l) = \nabla \cdot (D_m \nabla C_l)$$

$$C_m = \chi_s C_s + \chi_l C_l = \frac{m_s}{m} C_s + \frac{m_l}{m} C_l \Leftrightarrow m C_m = m_s C_s + m_l C_l \quad \rho_m C_m = r_s \rho_s C_s + r_l \rho_l C_l$$

$$\frac{m}{V} C_m = \frac{m_s}{V} C_s + \frac{m_l}{V} C_l \quad = r_s \rho_s k C_l + r_l \rho_l C_l$$

$$\rho_m C_m = \frac{m_s}{V} \frac{V_s}{V_s} C_s + \frac{m_l}{V} \frac{V_l}{V_l} C_l \quad = \rho_m C_l - r_s \rho_s (1-k) C_l$$

$$\frac{\partial(\rho_m C_l)}{\partial t} + \nabla \cdot (\rho_m \mathbf{v}_m C_l) = \nabla \cdot (D_m \nabla C_l) + \frac{\partial(r_s \rho_s (1-k) C_l)}{\partial t}$$

$$\frac{\partial(\rho_m C_l)}{\partial t} = \nabla \cdot (D_m \nabla C_l) + \frac{\partial(r_s \rho_s (1-k) C_l)}{\partial t}$$

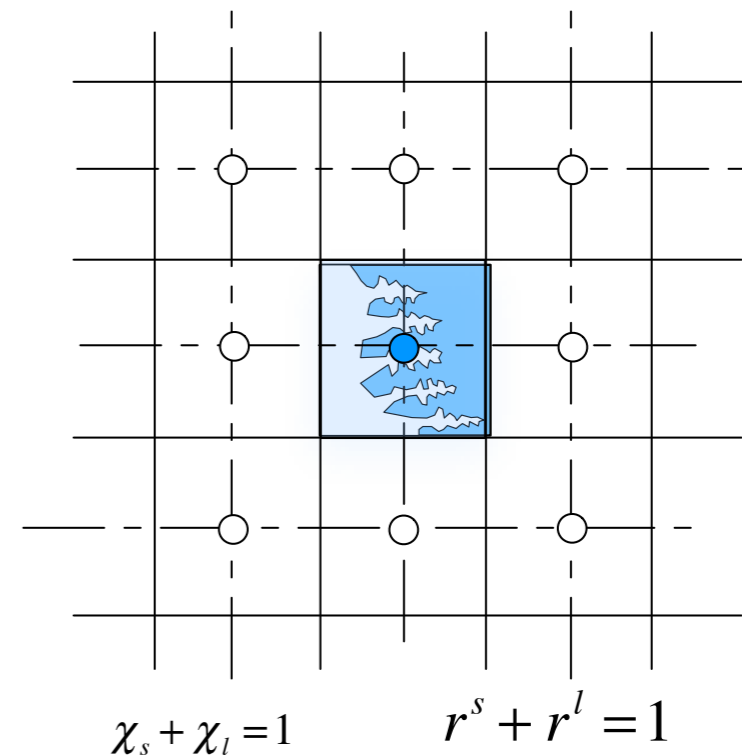
Case 1: no Specie diffusion

$$\frac{\partial(\rho_m C_m)}{\partial t} = 0$$

$$\frac{\partial(\rho_m c_{p,s} T)}{\partial t} = \nabla \cdot (k_m \nabla T) - \frac{\partial(r_l \rho_l \delta H)}{\partial t}$$

$$a_P T_P = \sum_{NB(P)} a_{NB} T_{NB} + b_P + a_P^t T_P^* - \frac{V \rho_l \delta H}{\Delta t} (r_{l,P} - r_{l,P}^*)$$

$$r_l = f(T) = \begin{cases} 1 & T > T_{Liquidus} \\ \frac{T - T_{Liquidus}}{T_{Liquidus} - T_{solidus}} & T_{solidus} < T < T_{Liquidus} \\ 0 & T < T_{solidus} \end{cases}$$



Liquid Fraction Update

$$a_P T_P = \sum_{NB(P)} a_{NB} T_{NB} + b_P + a_P^t T_P^* + \frac{V \rho_l \delta H}{\Delta t} (r_{l,P} - r_{l,P}^*)$$

$$\underline{T_P = f^{-1}(r_{l,P})}$$

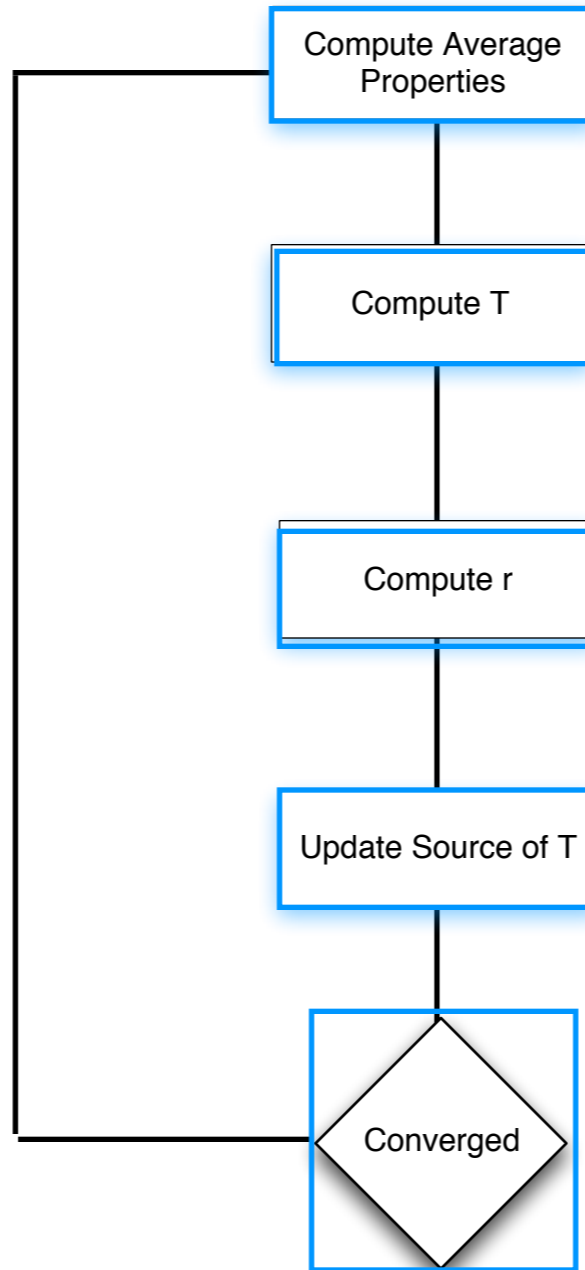
$$a_P f^{-1}(r_{l,P}) = \sum_{NB(P)} a_{NB} T_{NB} + b_P + a_P^t T_P^* - \frac{V \rho_l \delta H}{\Delta t} (r_{l,P} + \delta r_{l,P} - r_{l,P}^*)$$

$$\delta r_{l,P} = a_P \Delta t \frac{T_P - f^{-1}(r_{l,P})}{V \rho_l \delta H}$$

$$r_{l,P}^{n+1} = r_{l,P}^n + \delta r_{l,P}$$

$$0 \leq r_{l,P}^{n+1} \leq 1$$

Algorithm



case 2: Specie Diffusion

$$\frac{\partial(\bar{\rho}\bar{C})}{\partial t} + \nabla \cdot (r^s \tilde{\mathbf{v}}^s C_s + r^l \mathbf{v}^l C_l) = \nabla \cdot (r^s D^s \nabla C_s + r^l D^l \nabla C_l)$$

Under equilibrium conditions a discontinuity exist at the solid/liquid interface given by

$$C_l = C_s / k$$

$$C = \chi_l C_l + \chi_s C_s$$

$$\rho C = \rho_l \frac{V_l}{V} C_l + \rho_s \frac{V_s}{V} C_s$$

$$\chi_l = \frac{m_l}{m}$$

$$= \rho_l r_l C_l + \rho_s r_s k C_l$$

$$\chi_l = \frac{m_l}{m} = \frac{\rho_l V_l}{\rho V} = r_l \frac{\rho_l}{\rho}$$

$$\chi_l = \frac{C_l m C_s}{C_l - C_s}$$

$$mC = m_l C_l + m_s C_s$$

$$= (\rho - \rho_s r_s) C_l + \rho_s r_s k C_l$$

$$\rho = \rho_l r_l + \rho_s r_s$$

$$\rho V C = \rho_l V_l C_l + \rho_s V_s C_s$$

$$= \rho C_l - (1 - k) \rho_s r_s C_l$$

$$\rho = \rho_l \frac{V_l}{V} + \rho_s \frac{V_s}{V}$$

$$\rho C = \rho C_l - (1 - k) \rho_s r_s C_l$$

$$\frac{\partial(\bar{\rho}\bar{C})}{\partial t} + \nabla \cdot (r^s \tilde{\mathbf{v}}^s C_s + r^l \mathbf{v}^l C_l) = \nabla \cdot (r^s D^s \nabla C_s + r^l D^l \nabla C_l)$$

$$\rho V = \rho_l V_l + \rho_s V_s$$

$$\frac{\partial(\bar{\rho}\bar{C})}{\partial t} + \nabla \cdot (r^s \tilde{\mathbf{v}}^s C_s + r^l \mathbf{v}^l C_l) = \nabla \cdot (r^s D^s \nabla C_s + r^l D^l \nabla C_l)$$

$$r^s D^s \nabla C_s + r^l D^l \nabla C_l = (r^s D^s + r^l D^l k) \nabla C_l = \bar{D}^* \nabla C_l$$

$$\frac{\partial(\bar{\rho}C_l)}{\partial t} + \nabla \cdot (\bar{\rho} \mathbf{v}^* C_l) = \nabla \cdot (\bar{D}^* \nabla C_l)$$

Algorithm

Unknowns

T

r_l, r_s

χ_l, χ_s

C, C_l, C_s

Equations

Conservation of Energy (T)

Relations